

SINTESIS, KARAKTERISASI DAN AKTIVITAS KATALIS

Mg_{1-x}Zn_xF_{0,66}(OH)_{1,34} PADA REAKSI TRIMETILHIDROKUIKON DAN ISOFITOL

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Dosen Pembimbing :

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PENDAHULUAN

Katalis



PENDAHULUAN

TMHQ

+

Isofitol



Produk

Katalis

PENDAHULUAN

Katalis

Katalis + Homogen

H_2SO_4 , HCl, BF_3 , AlCl_3 dan FeCl_2/HCl
(Bonrath & Netscher, 2005)

- Sulit dipisahkan
- Korosif
- Katalis hanya bisa dipakai sekali (Lien, 2012)

Katalis Heterogen

Nafion/ SiO_2 (Laufer dkk., 2005), $\text{M}(\text{OTf})_3$
(Schrager & Bonrath, 2007)

- Mudah dipisahkan
- Tidak Korosif
- Katalis bisa dipakai kembali (Nguyen dkk., 2012)

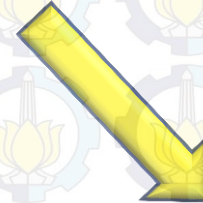
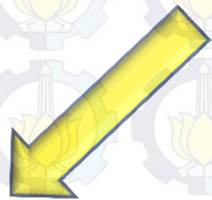
PENDAHULUAN

Keasaman Katalis

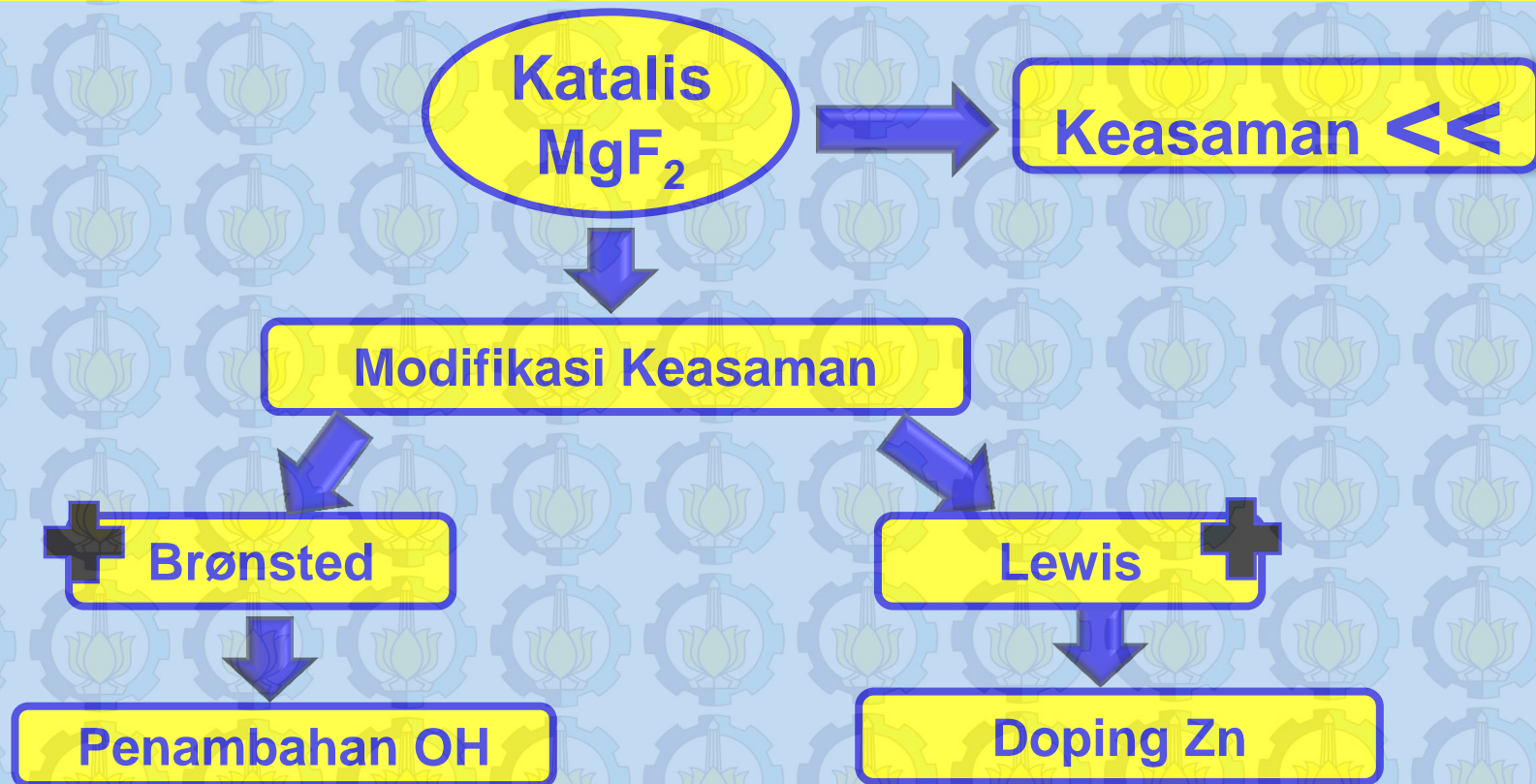
Asam Lewis

Asam Brønsted

Asam Lewis dan
Brønsted



RUMUSAN MASALAH



Keasaman

Konversi

Yield



TUJUAN PENELITIAN



* X = 0 ; 0,025 ; 0,05 ; 0,075 ; 0,1 ; 0,15

Aktivitas

TMHQ + Isofitol

Manfaat

Aplikasi pada reaksi TMHQ dan Isofitol

Sintesis Katalis



Karakterisasi

- XRD
- FTIR
- Adsorpsi Piridin-FTIR
- Adsorpsi gas N_2

Uji Katalisis

TMHQ + Isofitol

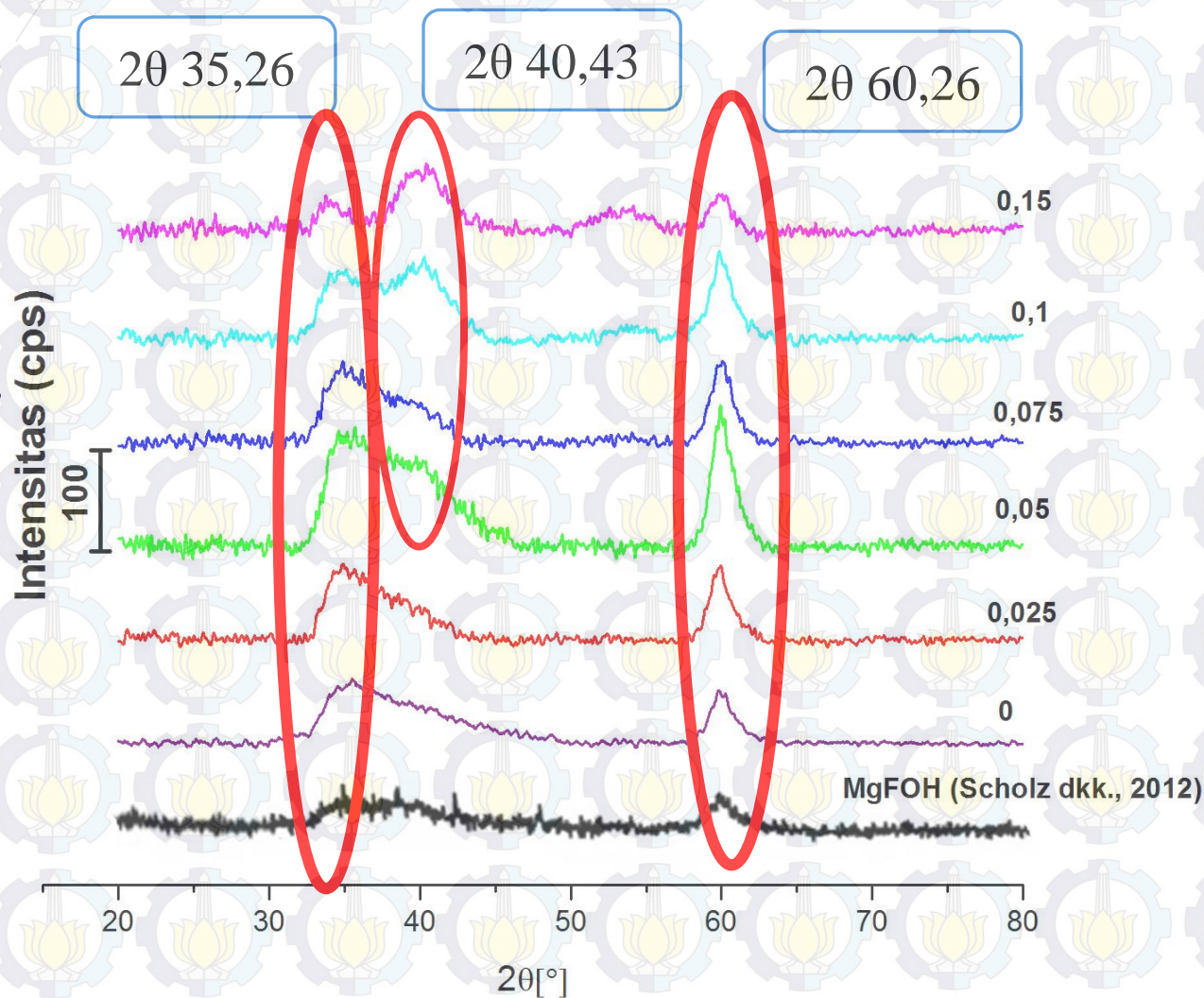


Produk



UV-Vis

* $x = 0 ; 0,025 ; 0,05 ; 0,075 ; 0,10$ dan $0,15$

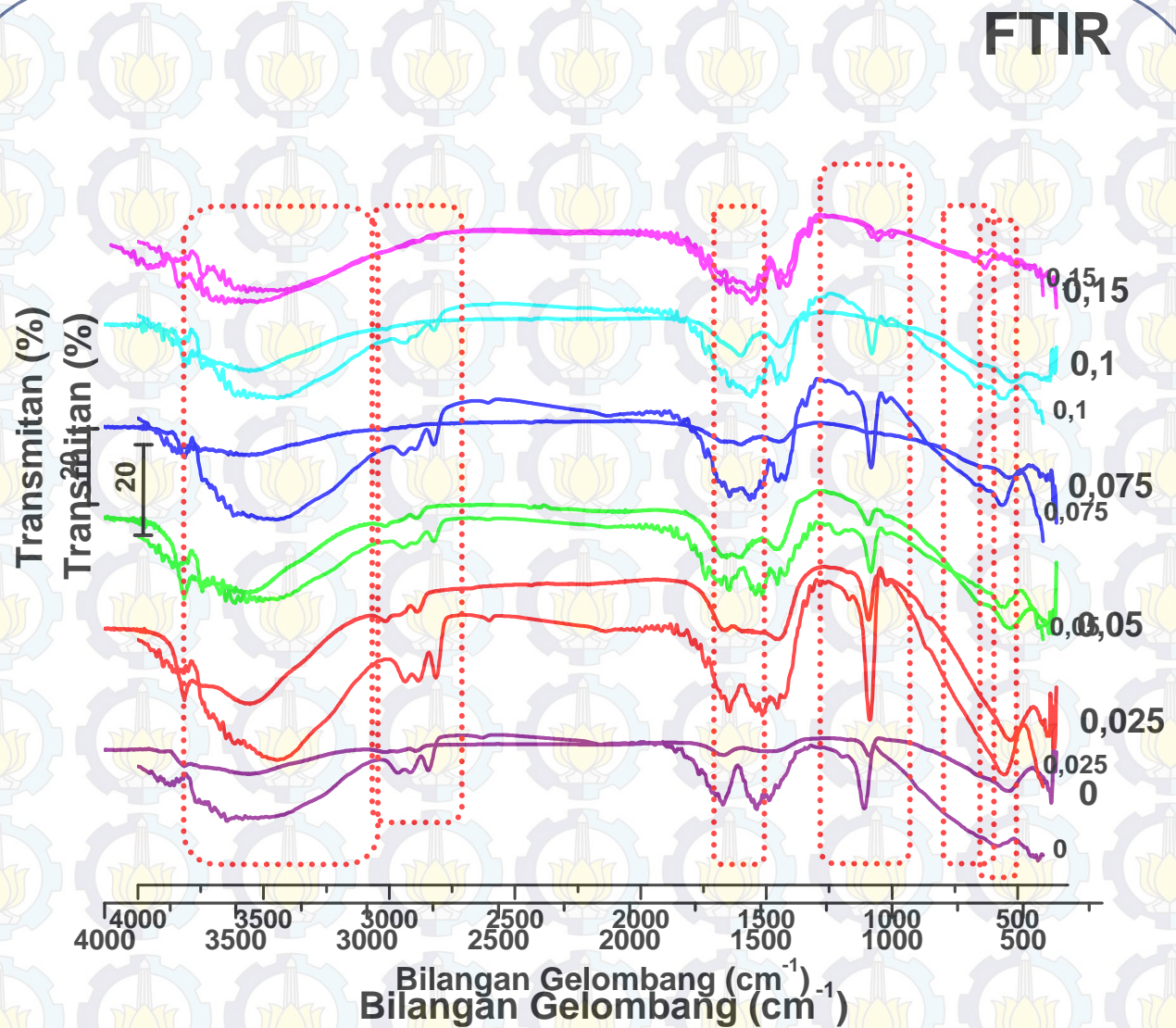
Difraktogram $\text{Mg}_{1-x}\text{Zn}_x\text{F}_{0,66}(\text{OH})_{1,34}$ 

Tabel pergeseran 2θ pada katalis $\text{Mg}_{1-x}\text{Zn}_x\text{F}_{0,66}(\text{OH})_{1,34}$

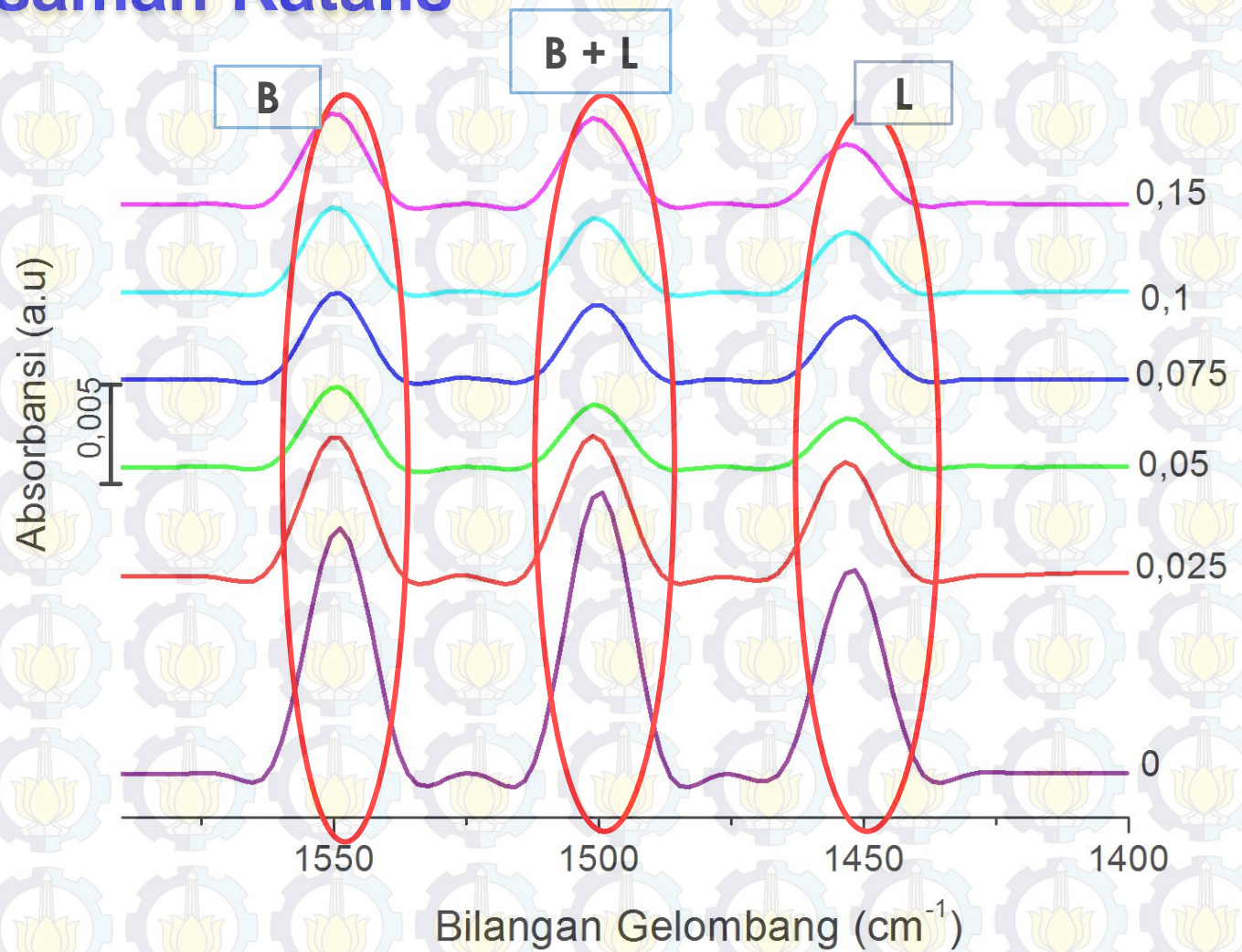
Nilai x pada katalis $\text{Mg}_{1-x}\text{Zn}_x\text{F}_{0,66}(\text{OH})_{1,34}$	Puncak 1		Puncak 2		Puncak 3	
	$2\theta(^{\circ})$	Int. (cps)	$2\theta(^{\circ})$	Int. (cps)	$2\theta(^{\circ})$	Int. (cps)
0	35,26	141	-	-	60,26	108
0,025	34,83	181	-	-	59,99	146
0,05	35,63	273	39,97	259	60,21	268
0,075	35,29	209	40,06	172	59,99	167
0,1	34,01	246	39,44	238	60,06	193
0,15	34,26	202	39,21	225	60,24	142

Sebelum
Kalsinasi

Setelah
Kalsinasi



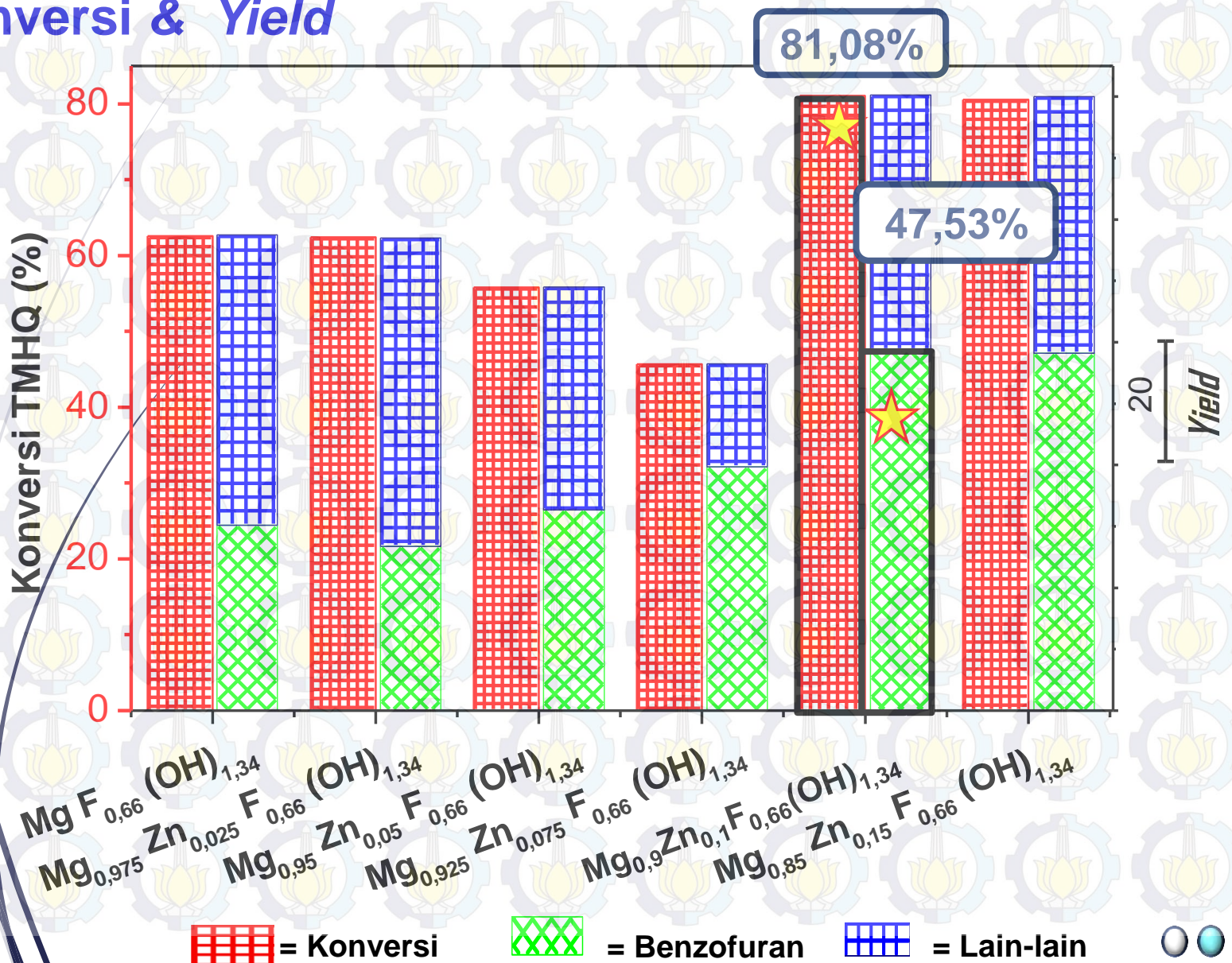
Profil Keasaman Katalis



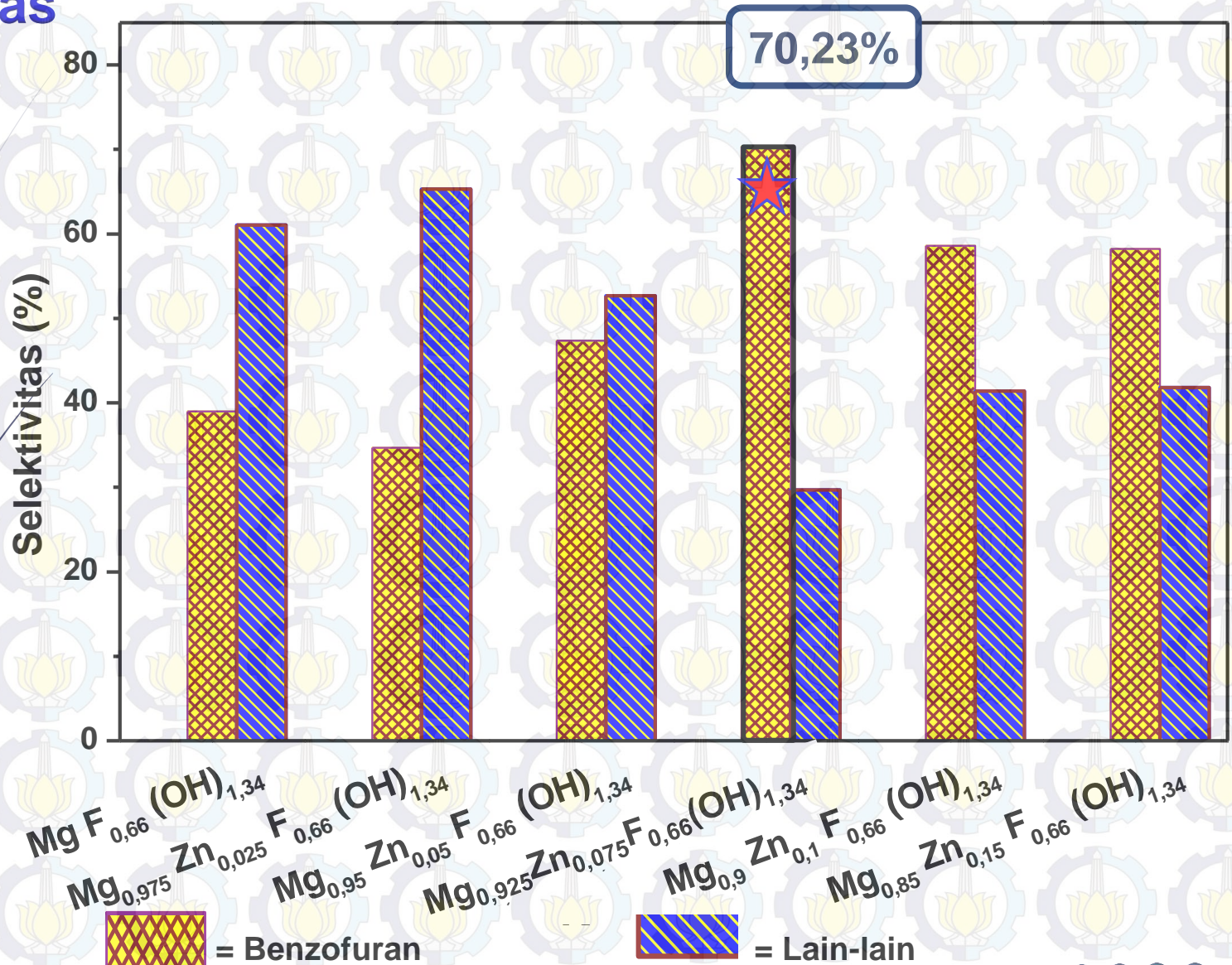
Luas Permukaan Katalis

Katalis	$S_{(BET)}$ (m ² /g)
$MgF_{0,66}(OH)_{1,34}$	26,884
$Mg_{0,975}Zn_{0,025}F_{0,66}(OH)_{1,34}$	202,757
$Mg_{0,95}Zn_{0,05}F_{0,66}(OH)_{1,34}$	369,603
$Mg_{0,925}Zn_{0,075}F_{0,66}(OH)_{1,34}$	308,079
$Mg_{0,9}Zn_{0,1}F_{0,66}(OH)_{1,34}$	253,720
$Mg_{0,85}Zn_{0,15}F_{0,66}(OH)_{1,34}$	236,325

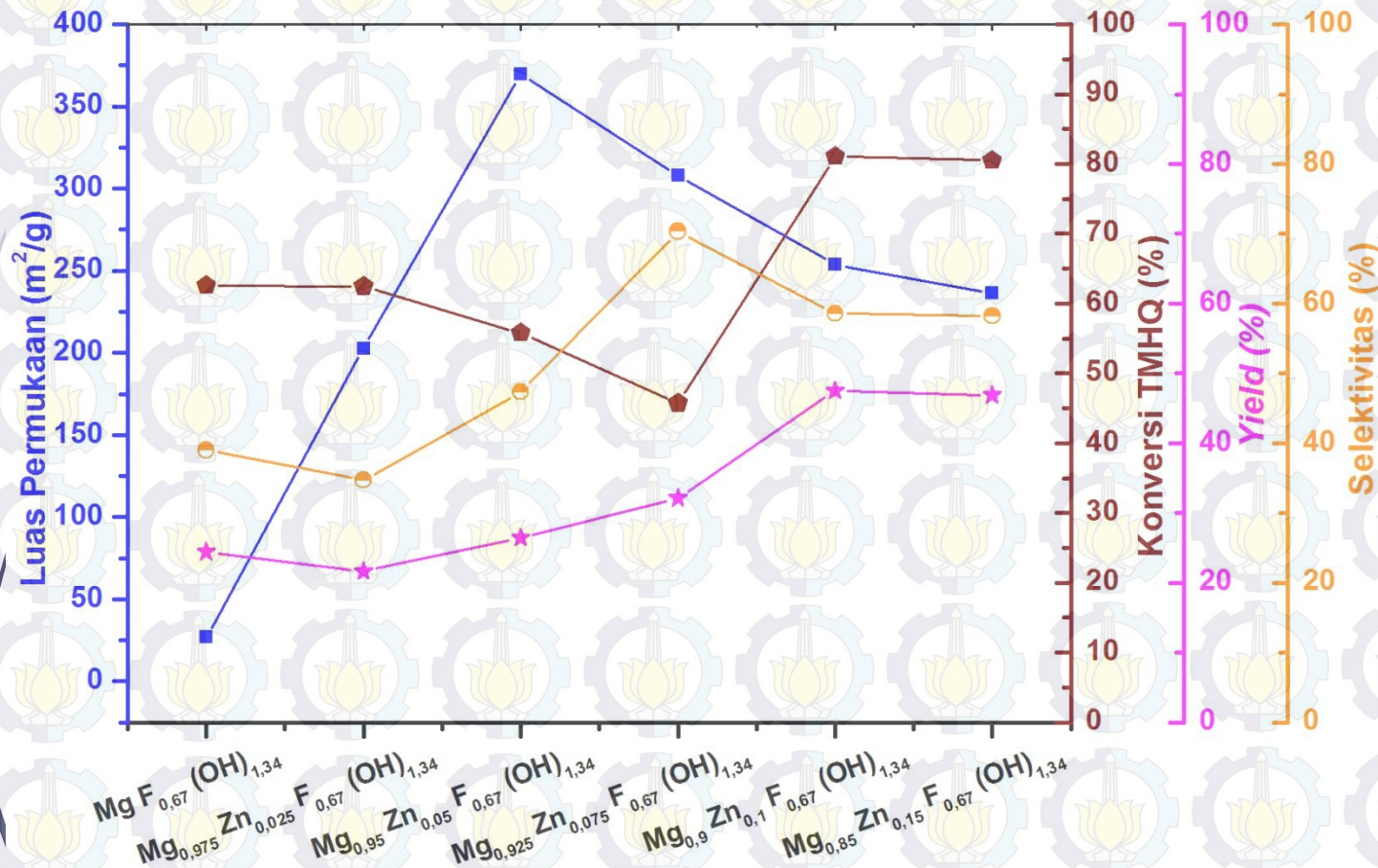
Konversi & Yield



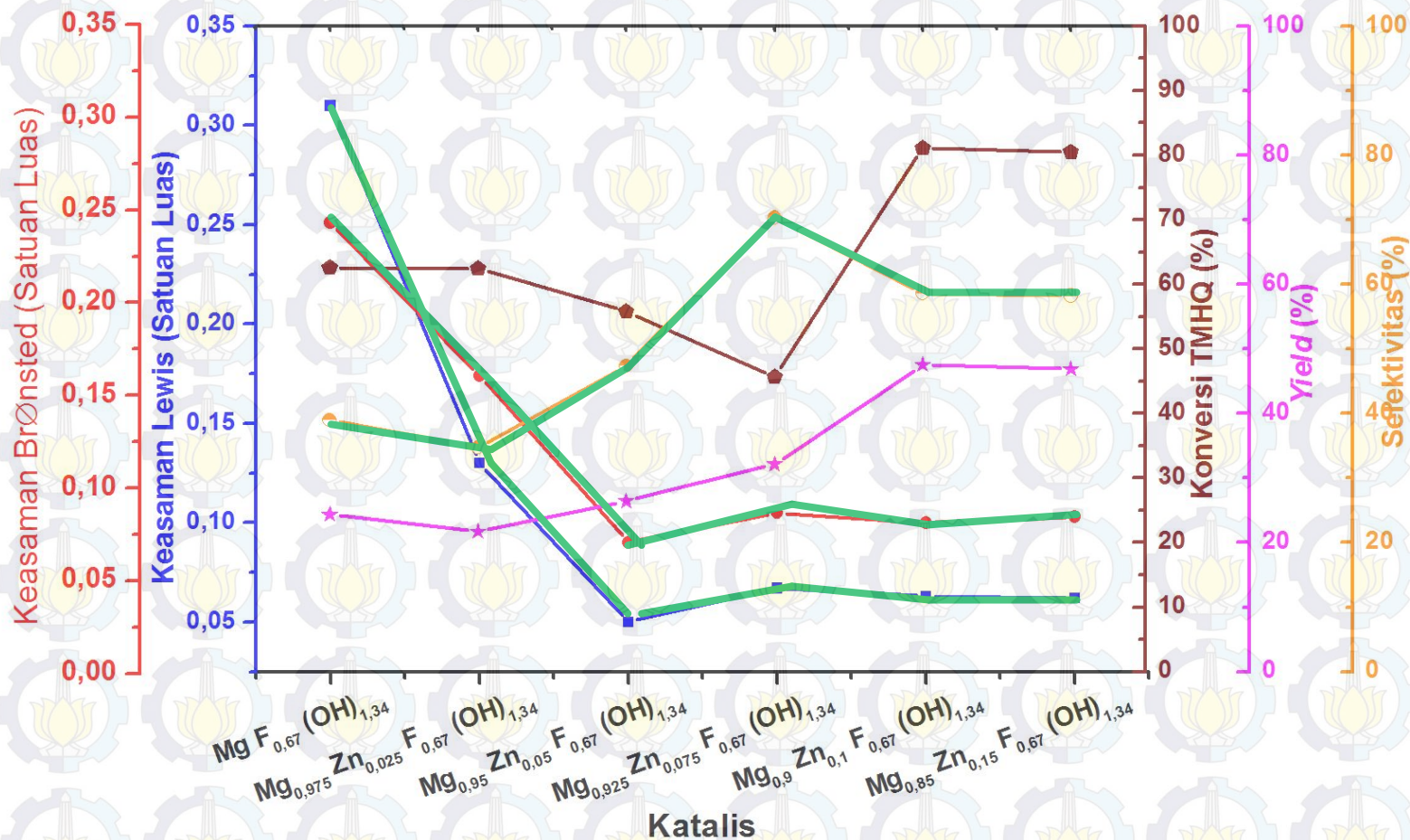
Selektivitas



Korelasi antara luas permukaan pada katalis dengan konversi TMHQ, *yield* dan selektivitas benzofuran



Korelasi antara keasaman katalis dengan konversi TMHQ, *yield* dan selektivitas benzofuran



KESIMPULAN



X= 0

X= 0,025

X= 0,05

X= 0,075

X= 0,1

X= 0,15

Konversi TMHQ

Yield

Selektivitas

81,08%

47,53 %

Benzofuran

Benzofuran

70,32%

Keasaman Katalis

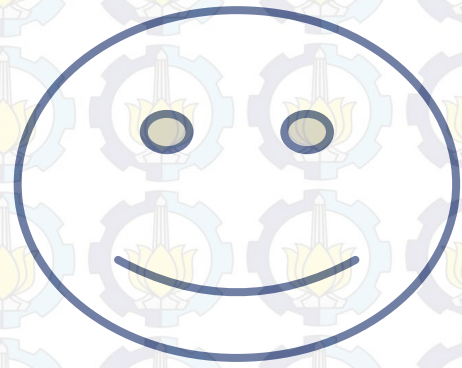
Luas Permukaan

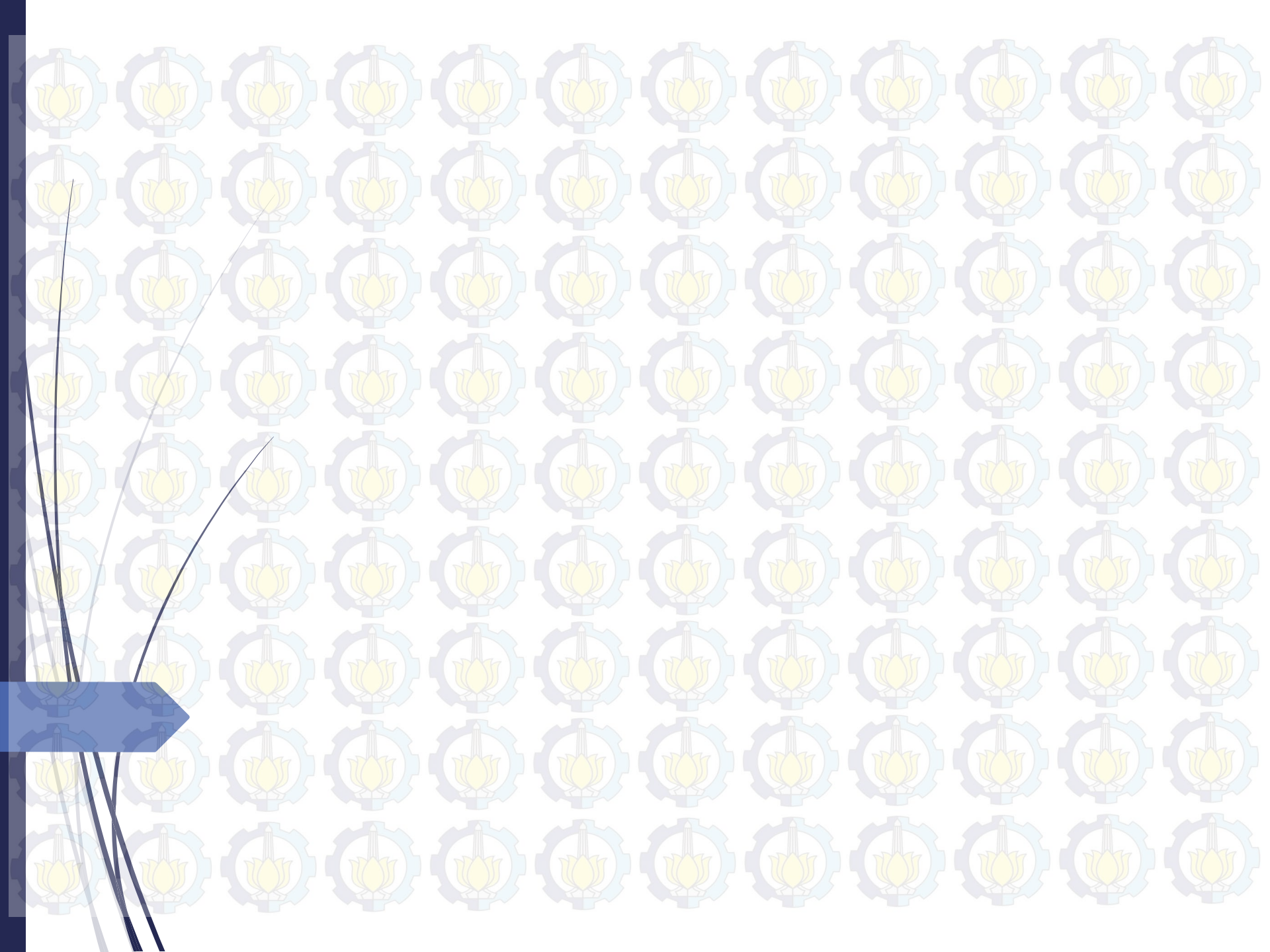
TERIMA KASIH

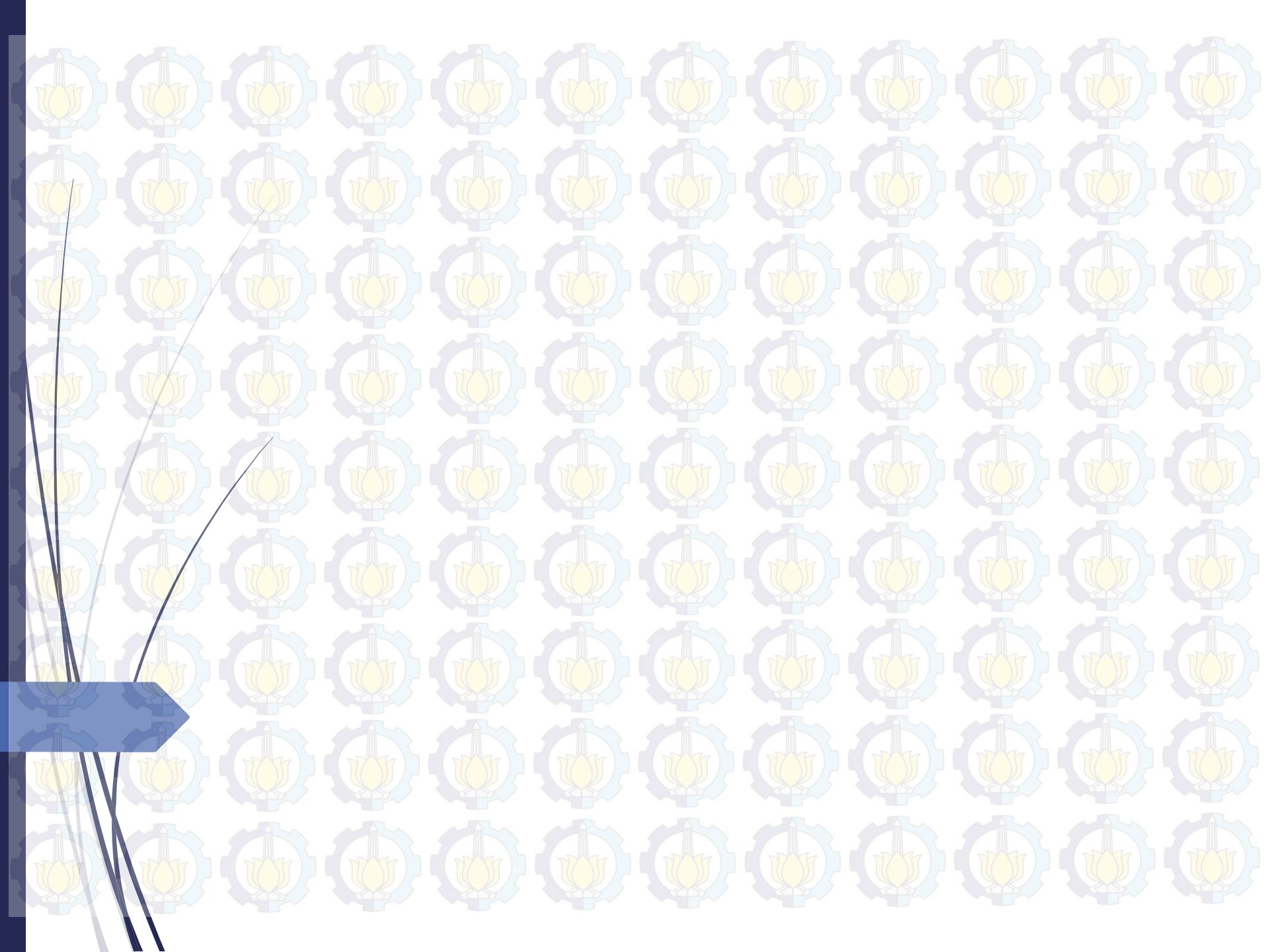
- ✓ Prof. Dr. rer. nat. Irmina Kris Murwani
- ✓ Tim Dosen Penguji
- ✓ Tim Penelitian Katalis Heterogen
- ✓ Semua pihak yang telah mendukung dalam penyusunan Tugas Akhir ini

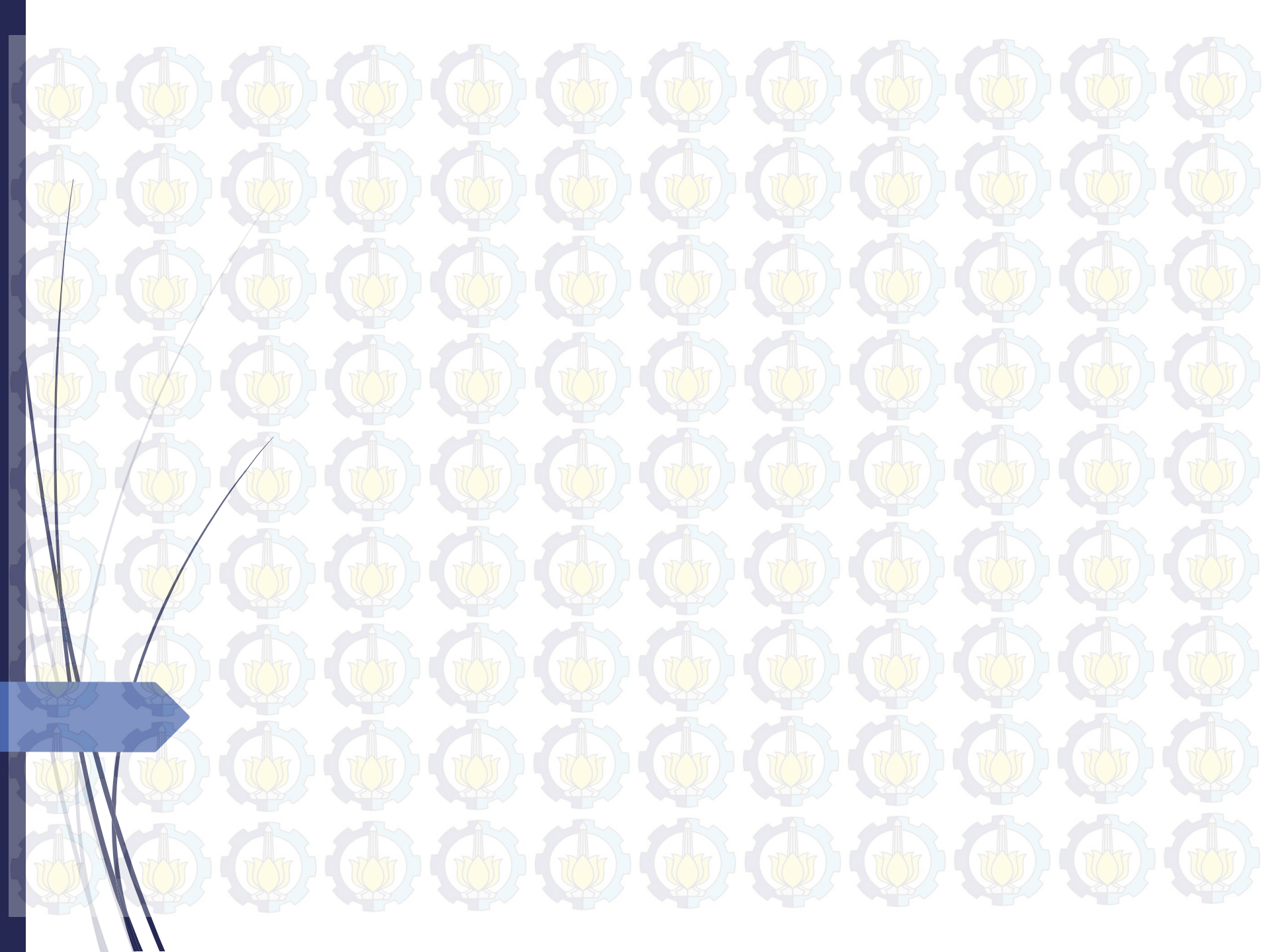


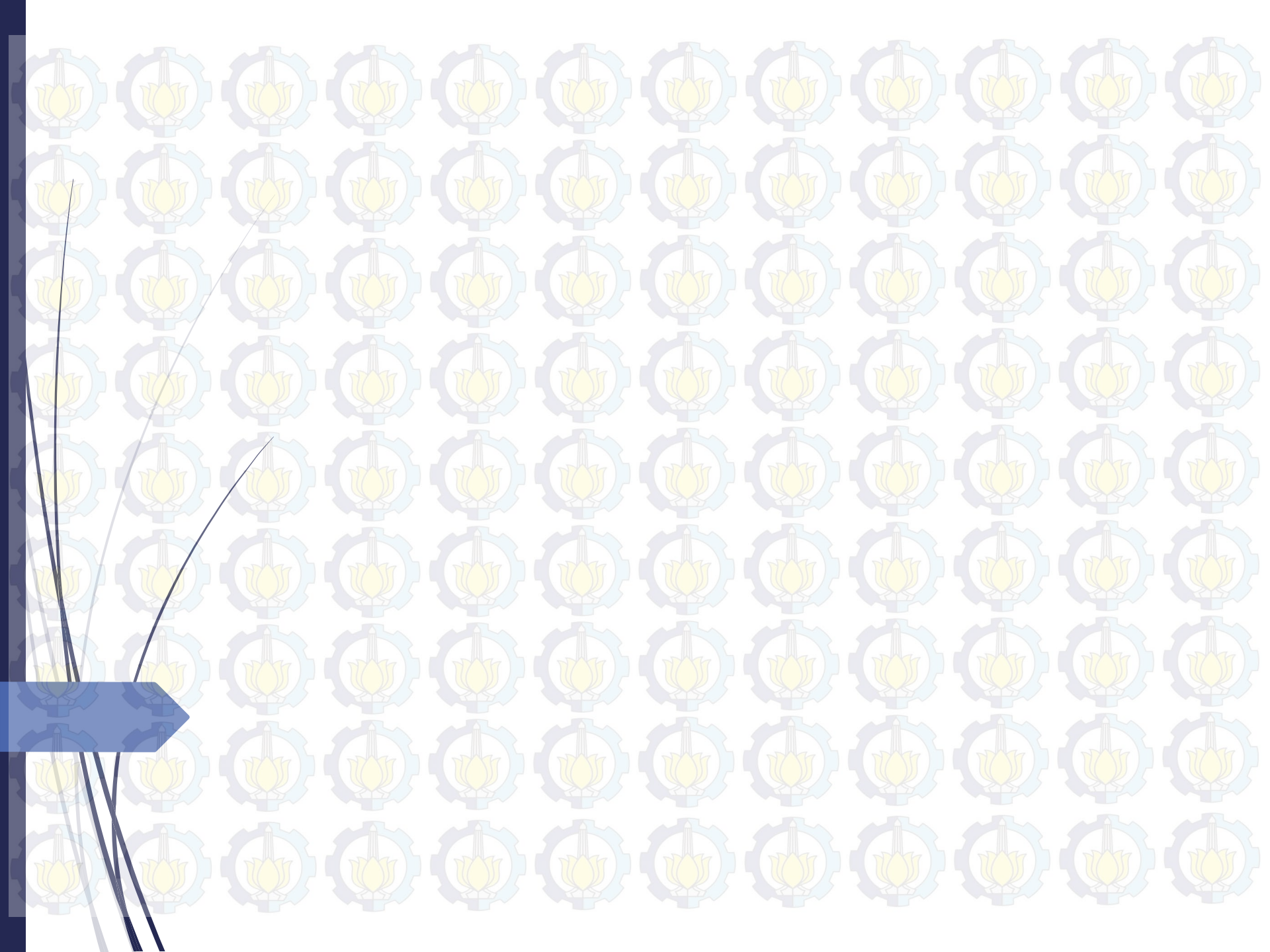
Terima Kasih

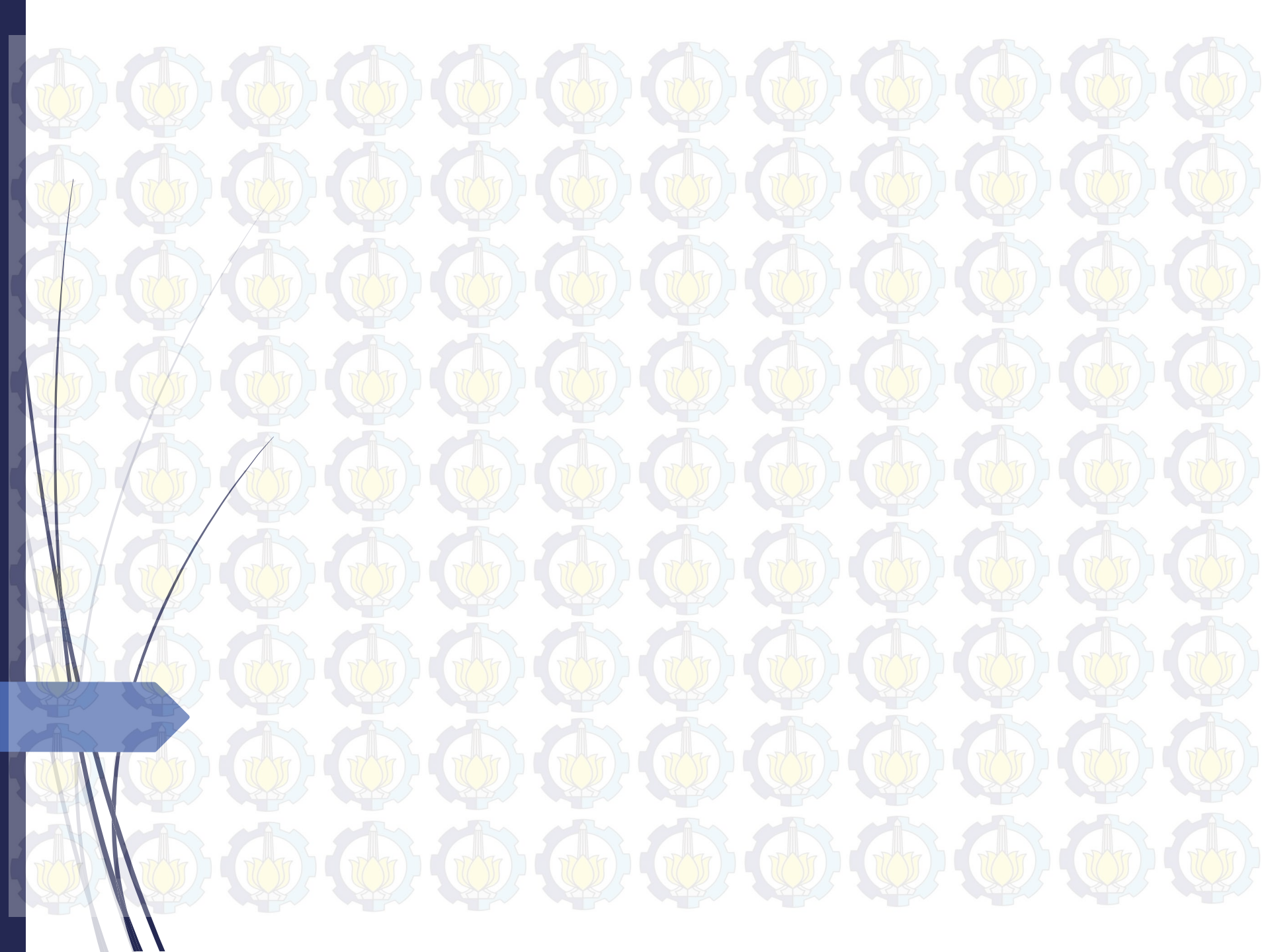


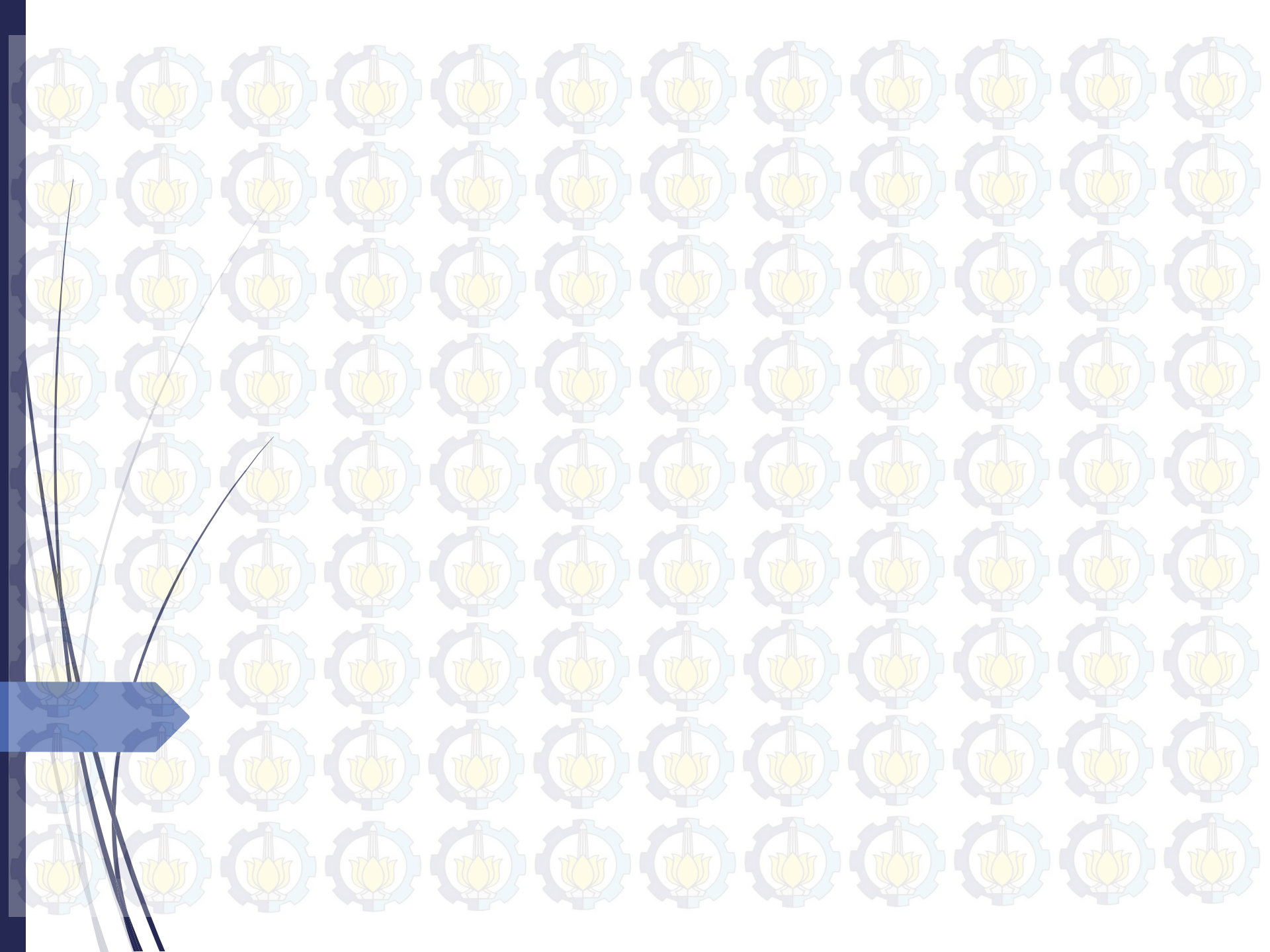


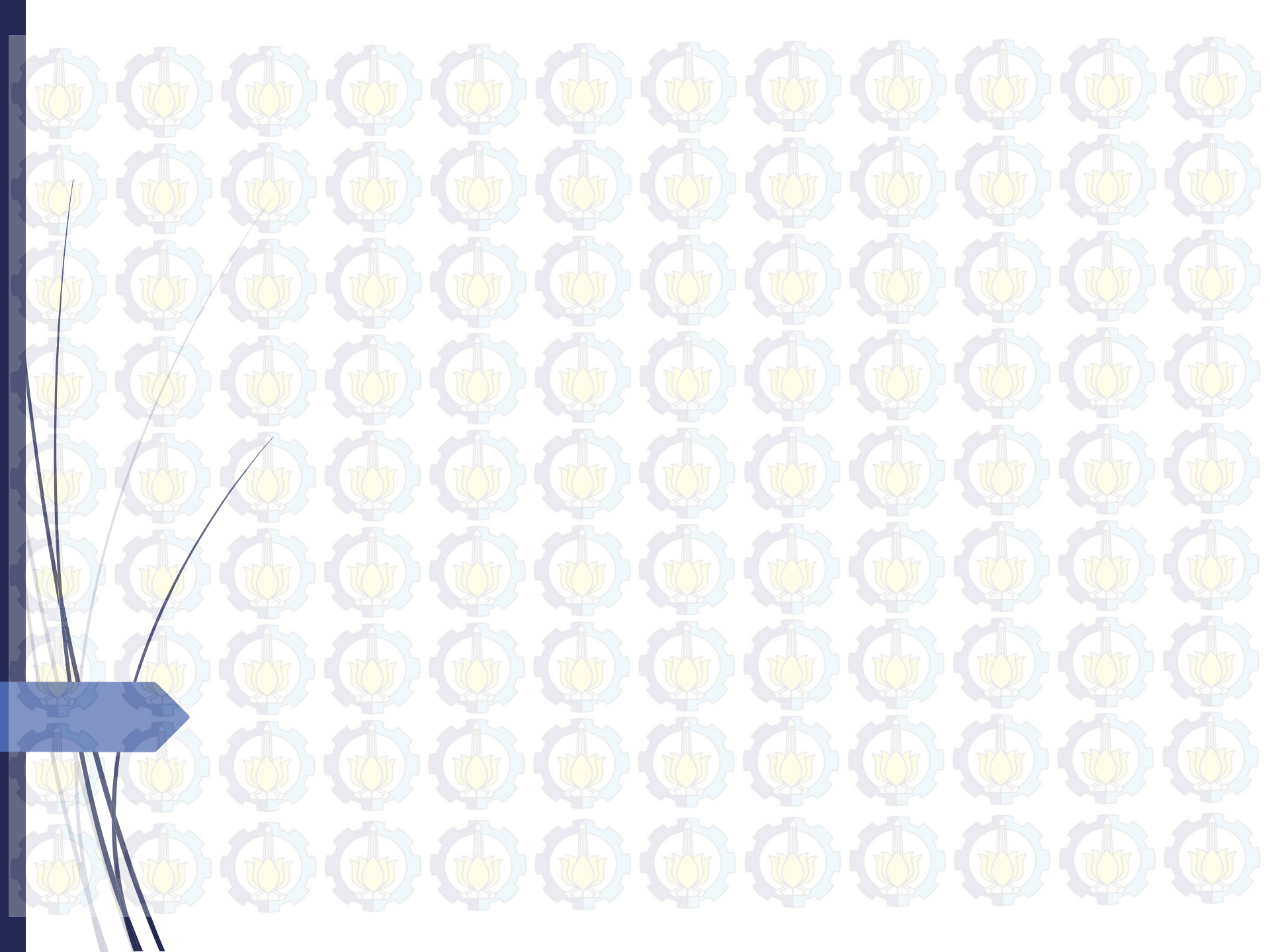


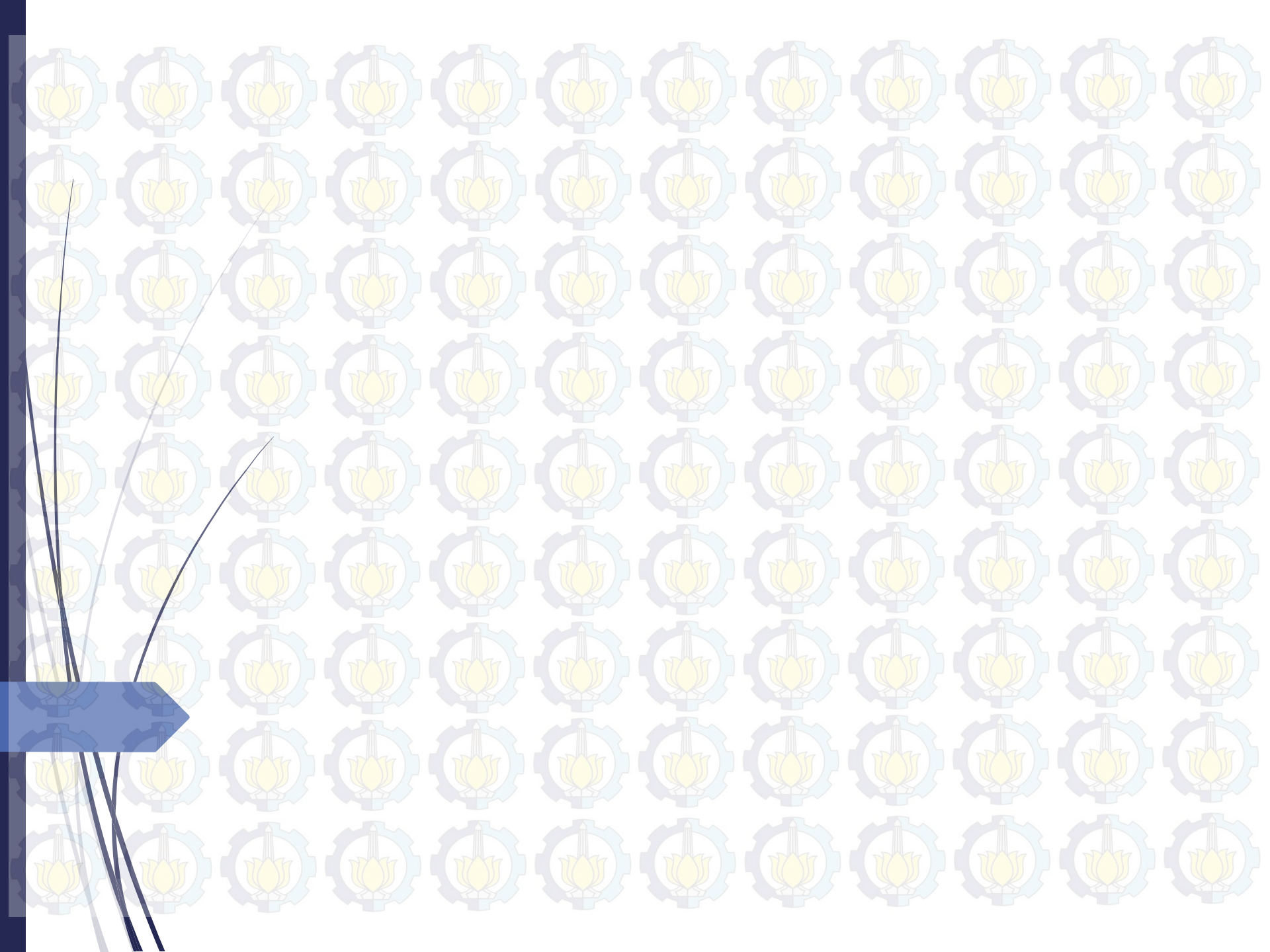






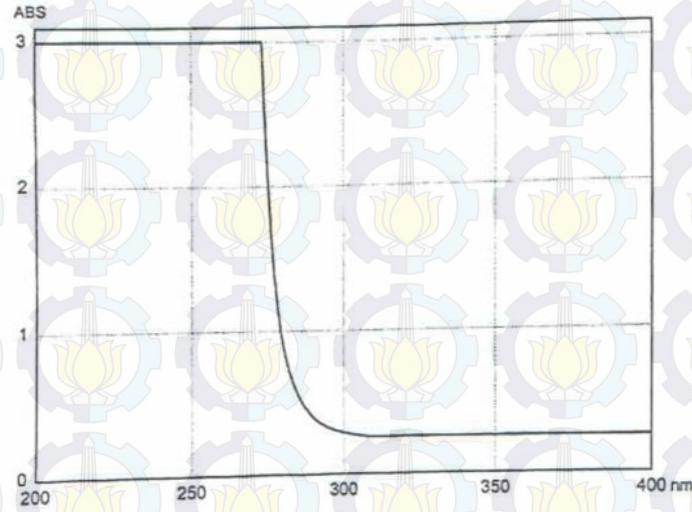






UV1100 Spectrophotometer

Serial NUM: 5210027
ROM Version: 20
Sample Name:
Date:
Operator:



Wavelength Scan
Data Mode: ABS
Scan Range: 400.0-200.0nm
Slit Width: 4nm
Speed (nm/min) : 200nm/min
Lamp Change Wavelength: 340.0nm
Path Length:

Peak WL (nm)	ABS	WL (nm)	ABS

UV1100 Spectrophotometer

Serial NUM: 5210027

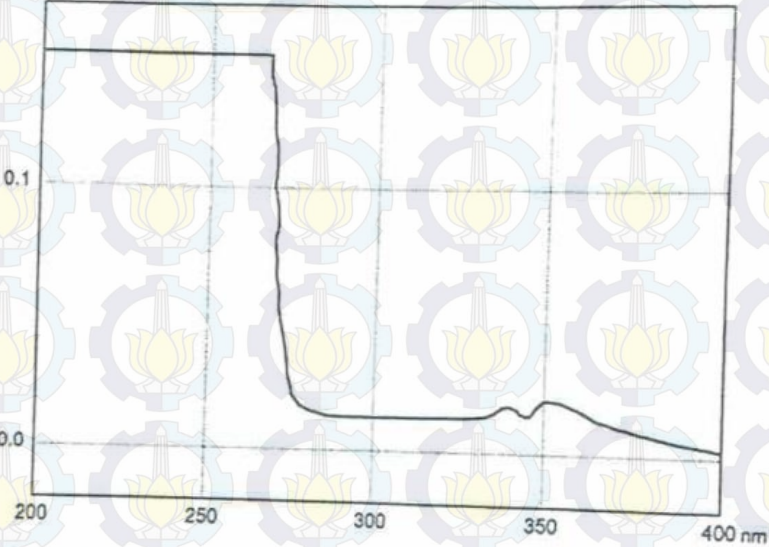
ROM Version: 20

Sample Name:

Date:

Operator:

ABS



Wavelength Scan

Data Mode:

Scan Range:

Slit Width:

Speed (nm/min) :

Lamp Change Wavelength:

Path Length:

ABS

400.0-200.0nm

4nm

200nm/min

340.0nm

Peak

WL (nm)

338.0

ABS

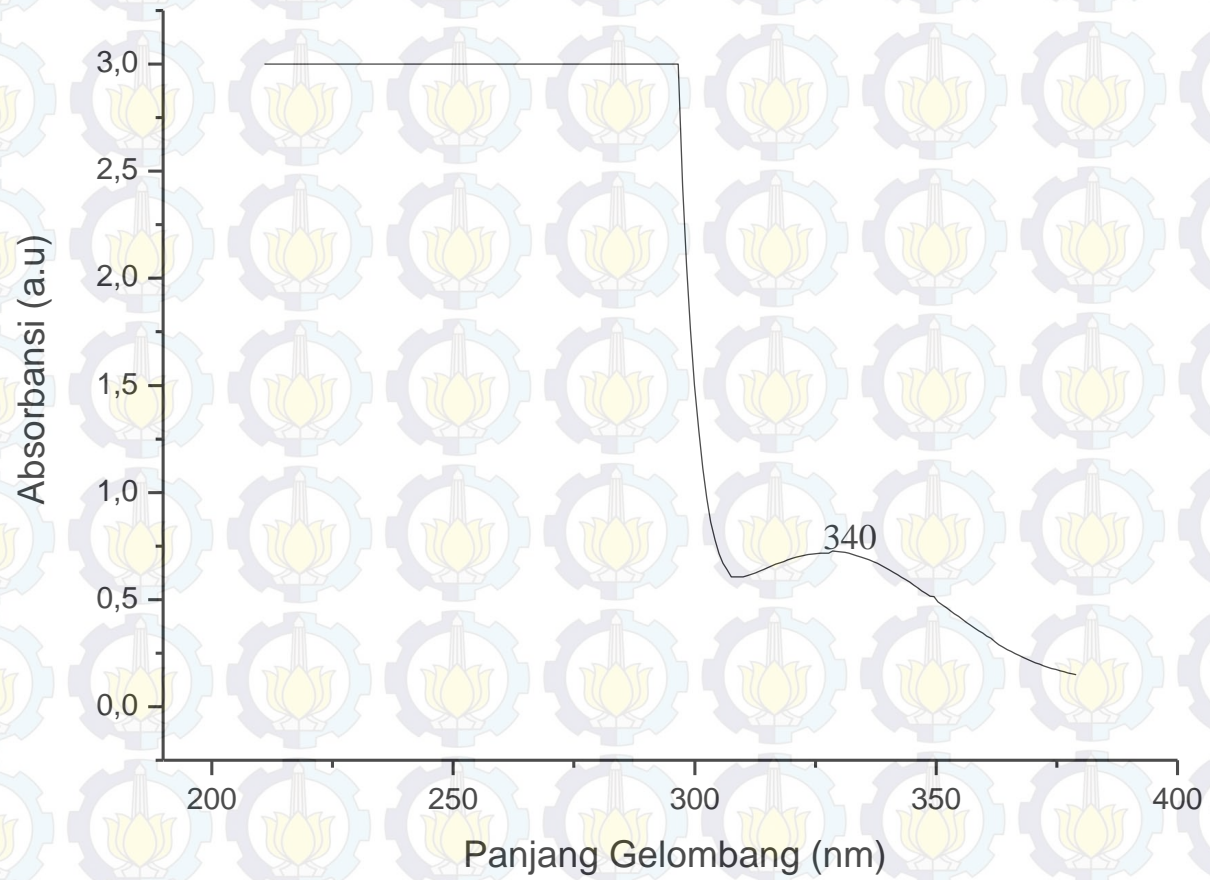
0.0165

WL (nm)

352.8

ABS

0.0253



Katalis

Absorbansi



0,025



0,029



0,037

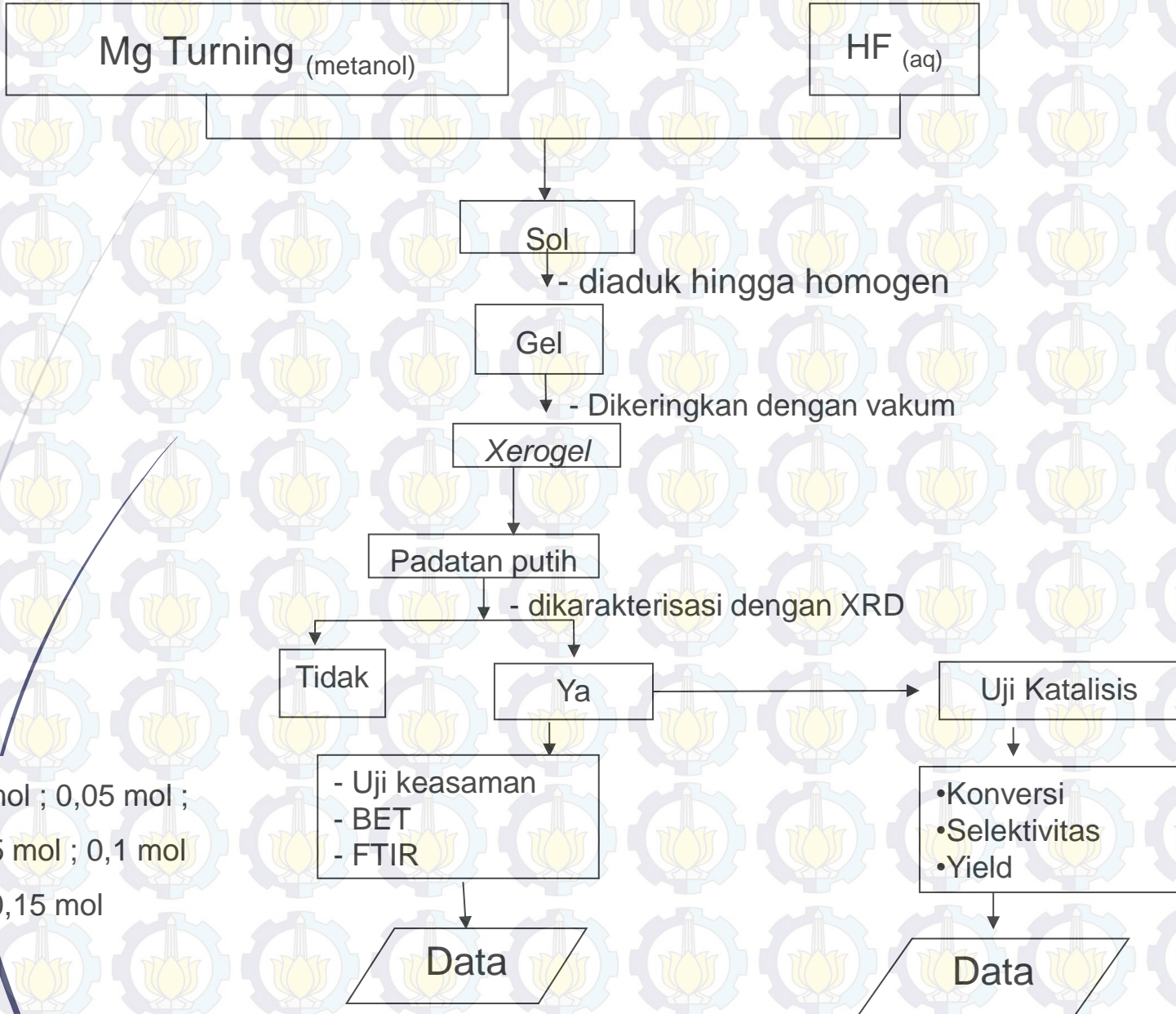


0,011



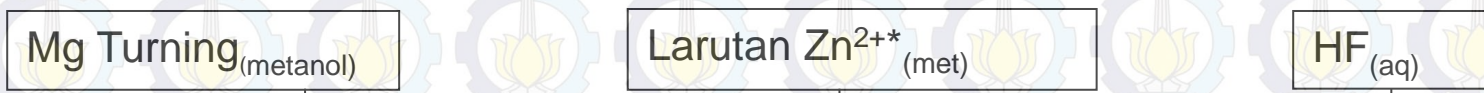
0,012

Sintesis $MgF_{0,66}(OH)_{1,34}$



0,025 mol ; 0,05 mol ;
0,075 mol ; 0,1 mol
dan 0,15 mol

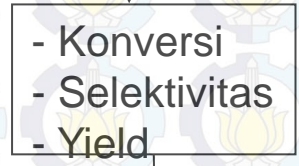
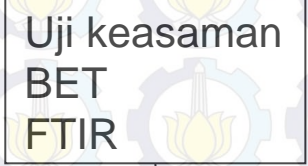
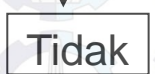
Sintesis Katalis $Mg_{1-x}Zn_xF_{0,66}(OH)_{1,34}$



Dikeringkan dengan vakum

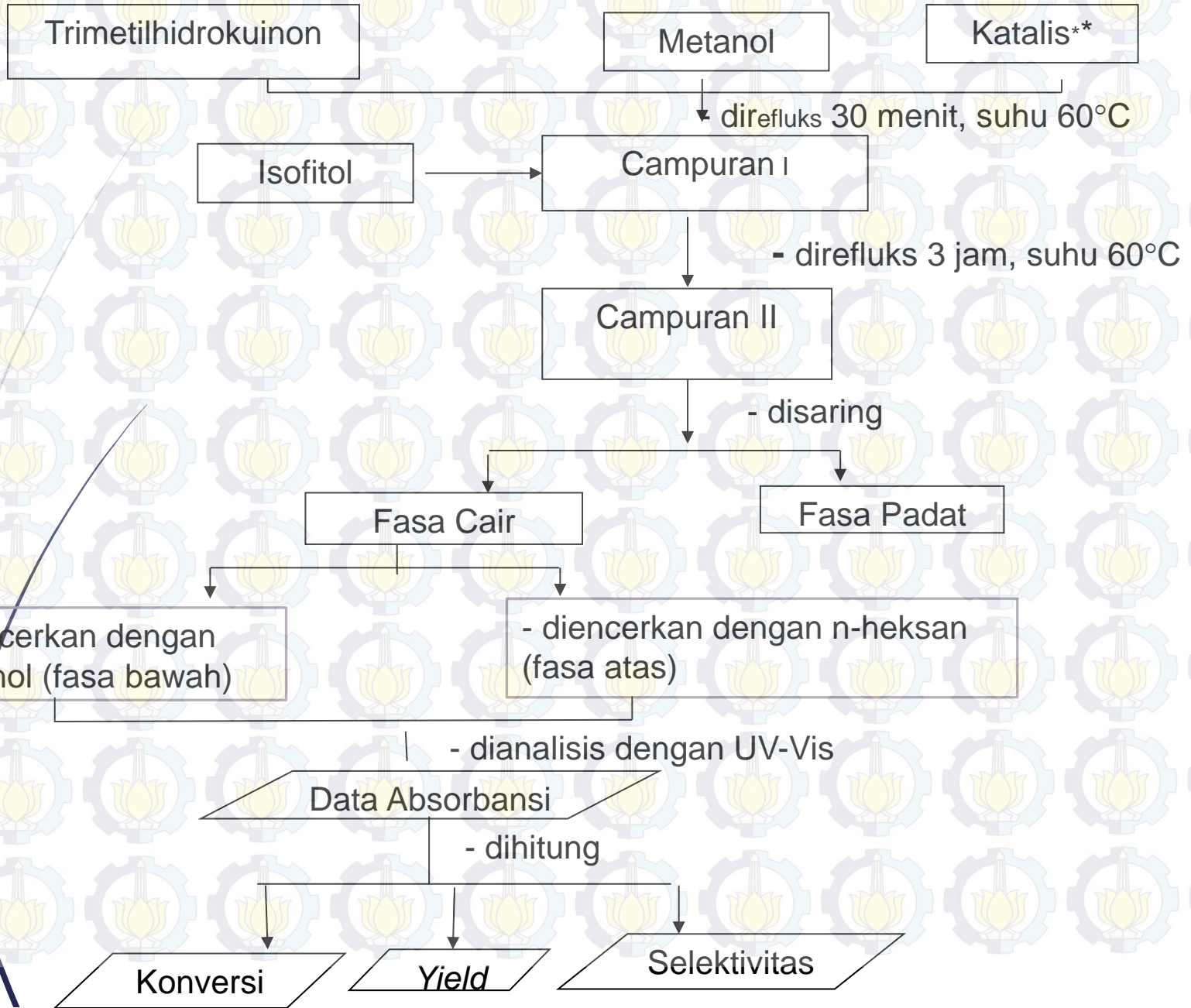


Dikarakterisasi dengan XRD



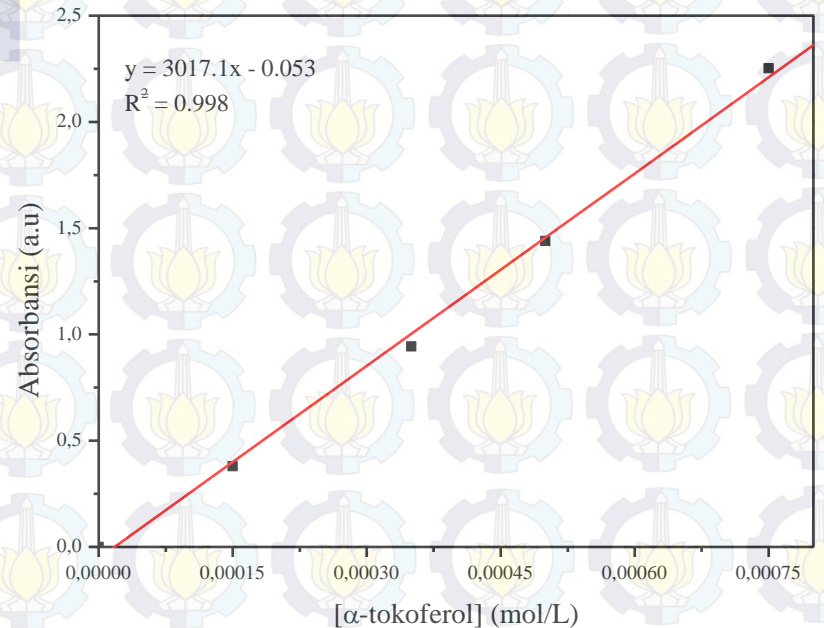
•0,025 mol ; 0,05 mol ;
0,075 mol ; 0,1 mol
dan 0,15 mol

Uji Katalisis pada Reaksi antara Trimetilhidrokuinon dan Isofitol



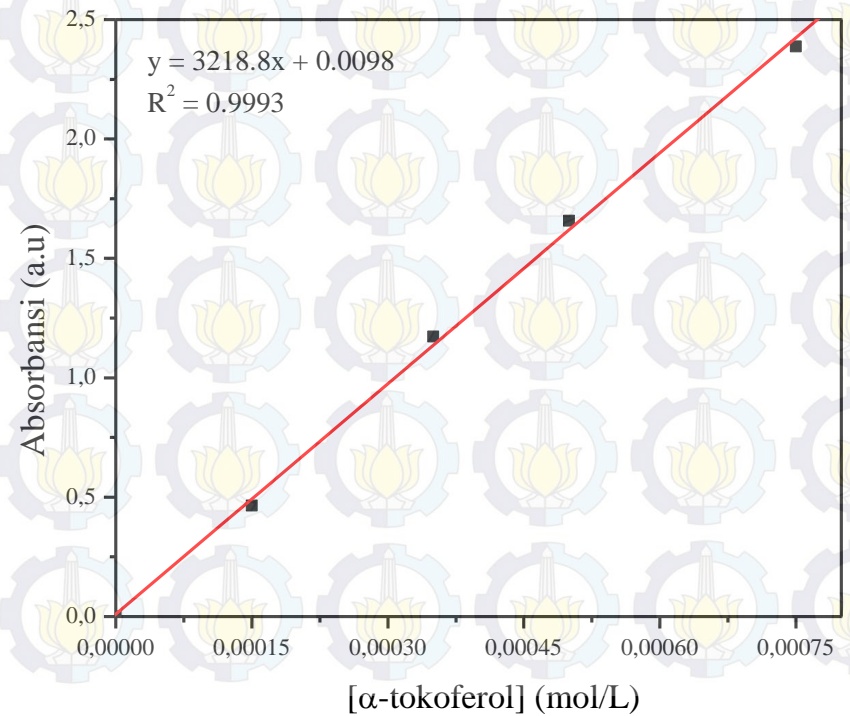
•Kurva Kalibrasi α -tokoferol dalam Metanol

Konsentrasi α -tokoferol (mol/L)	Absorbansi (a.u)
0	0
0,00016	0,00871
0,00048	0,03114
0,0008	0,05776
0,00112	0,078



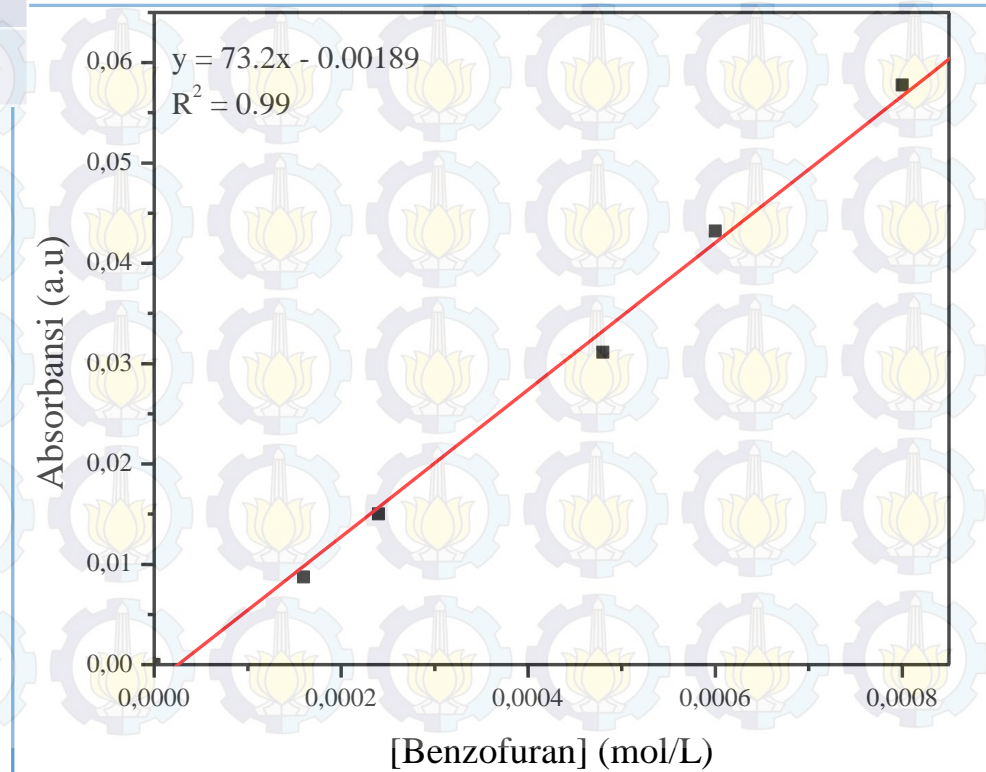
•Kurva Kalibrasi α -tokoferol dalam n-heksana

Konsentrasi α -tokoferol (mol/L)	Absorbansi (a.u)
0	0
0,00015	0,465
0,00035	1,172
0,0005	1,658
0,00075	2,387



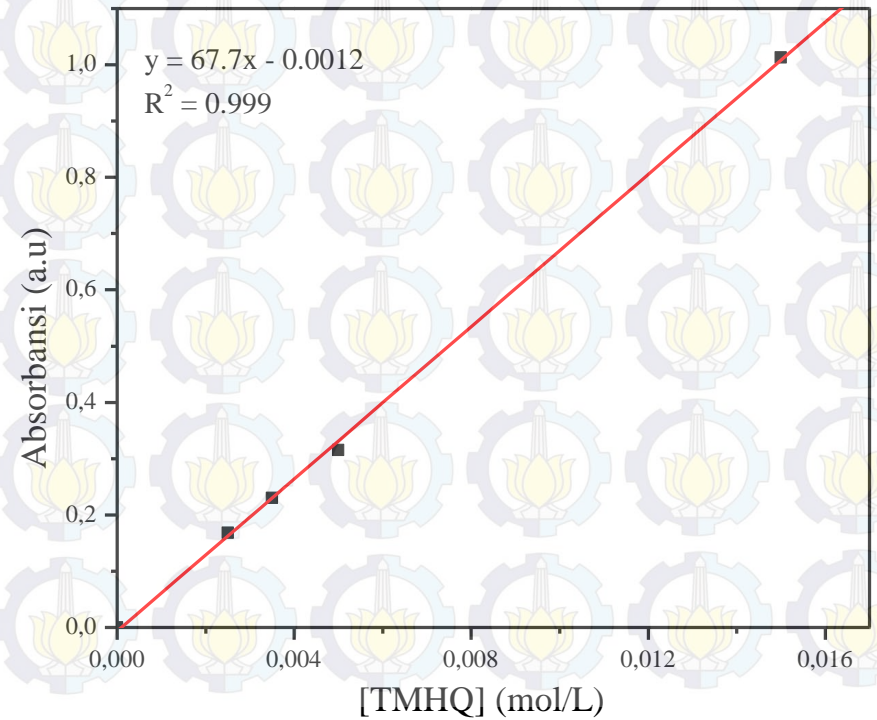
•Kurva Kalibrasi Benzofuran dalam Metanol

Konsentrasi Benzofuran (mol/L)	Absorbansi (a.u)
0	0
0,00016	0,00871
0,00024	0,015
0,00048	0,03114
0,0006	0,0432
0,0008	0,05776



•Kurva Kalibrasi TMHQ dalam Metanol

Konsentrasi TMHQ (mol/L)	Absorbansi (a.u)
0	0
0,0025	0,168
0,0035	0,23
0,005	0,315
0,015	1,013



Pengukuran absorbansi TMHQ pada $\lambda = 352,8 \text{ nm}$ adalah 0,025

$V = 10 \text{ mL} = 0,01 \text{ L}$

TMHQ_{awal}

Persamaan regresi linear TMHQ yang diperoleh :

$$y = 67,7x - 0,0012$$

dimana :

$$y = A + Bx$$

dengan, $x = \text{Konsentrasi (mol/L)}$

$y = \text{Absorbansi}$

$$\text{mol TMHQ sisa} = 0,000387 \text{ mol/L} \times 0,01 \text{ L} \times 10$$

$$= 0,0000387 \text{ mol}$$

$$= 0,0387 \text{ mmol}$$

Konversi atau Aktivitas

Yield dan Selektivitas

Pengukuran absorbansi benzofuran pada $\lambda = 338 \text{ nm}$ adalah 0,0142.

$$V = 10 \text{ mL} = 0,01 \text{ L}$$

Persamaan regresi linear α -tokoferol yang diperoleh :

$$y = 73,2x - 0,00189$$

dimana :

$$y = A + Bx$$

dengan, $x = \text{Konsentrasi (mol/L)}$

$y = \text{Absorbansi}$

$$\text{mol benzofuran} = 0,000219 \text{ mol/L} \times 0,01 \text{ L} \times 10$$

$$= 0,0000219 \text{ mol}$$

$$= 0,0219 \text{ mmol}$$

Yield

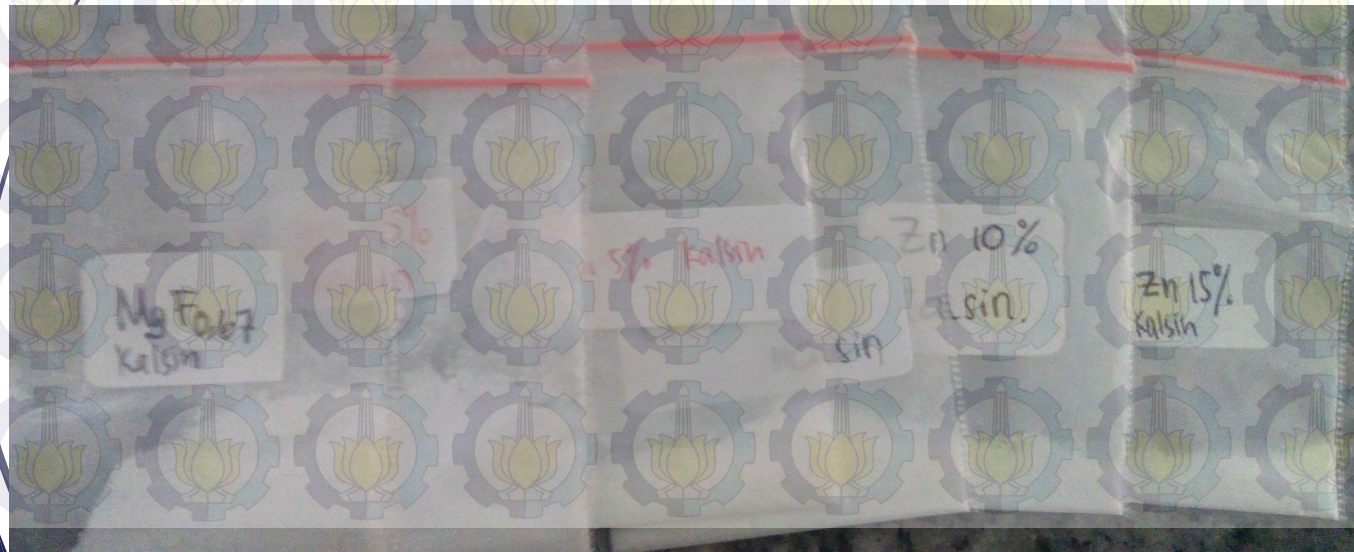
$$= 21,89 \%$$

Selektivitas

Sebelum kalsinasi



Setelah kalsinasi



Katalis	Konversi (%)	Yield (%)	
		Benzofuran	Lain-lain
$\text{MgF}_{0,67}(\text{OH})_{1,34}$	62,582440	24,389828	38,192612
$\text{Mg}_{0,975}\text{Zn}_{0,025}\text{F}_{0,67}(\text{OH})_{1,3}$ 4	62,443283	21,666088	40,777195
$\text{Mg}_{0,95}\text{Zn}_{0,05}\text{F}_{0,67}(\text{OH})_{1,34}$	55,802965	26,417057	29,385908
$\text{Mg}_{0,925}\text{Zn}_{0,075}\text{F}_{0,67}(\text{OH})_{1,3}$ 4	45,693346	32,132467	13,560878
$\text{Mg}_{0,9}\text{Zn}_{0,1}\text{F}_{0,67}(\text{OH})_{1,34}$	81,079821	47,525754	33,554067
$\text{Mg}_{0,85}\text{Zn}_{0,15}\text{F}_{0,67}(\text{OH})_{1,34}$	80,533304	46,876282	33,657022

Katalis

Selektivitas (%)

Benzofuran

Lain-Lain



38,972319

61,027681



34,697227

65,302773



47,339881

52,660119



70,321984

29,678016



58,616007

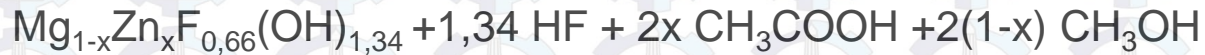
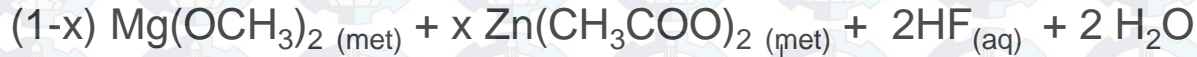
41,383993



58,207325

41,792675

Perhitungan Sintesis $Mg_{1-x}Zn_xF_{0,66}(OH)_{1,34}$



❑ Massa senyawa target = 2 g

❖ Menghitung Mr produk

$$\begin{array}{r} Mg = 0,975 \times 24,38 = 23,4 \\ Zn = 0,025 \times 65,37 = 1,63 \\ F = 0,66 \times 19 = 12,54 \\ \hline OH = 1,34 \times 17 = 22,78 \\ \hline = 60,35 \text{ g/mol} \end{array} +$$

$$\text{Mol Produk} = \frac{2}{60,35} = 0,033 \text{ mol}$$

$$\text{Kebutuhan Mg Turning} = 0,975 \times 0,033 \times 24,3 = 0,782 \text{ g}$$

$$\text{Kebutuhan HF} = \frac{0,033}{27,12} \times 0,67 \times 1000 = 0,82 \text{ mL}$$

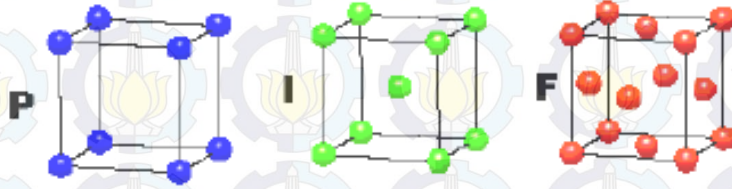
$$\text{Kebutuhan Logam Zn} = 0,025 \times 0,033 \times 219,49 = 0,1811$$

Geometri kristal

CUBIC

$$a = b = c$$

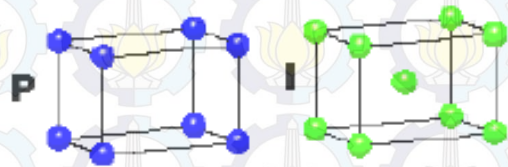
$$\alpha = \beta = \gamma = 90^\circ$$



TETRAGONAL

$$a = b \neq c$$

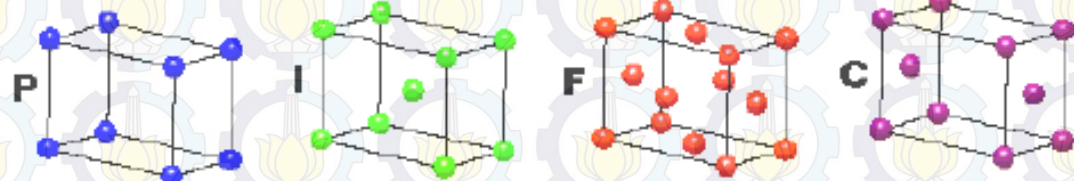
$$\alpha = \beta = \gamma = 90^\circ$$



ORTHORHOMBIC

$$a \neq b \neq c$$

$$\alpha = \beta = \gamma = 90^\circ$$



HEXAGONAL

$$a = b \neq c$$

$$\alpha = \beta = 90^\circ$$

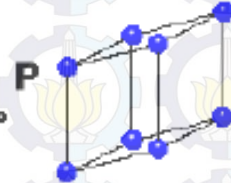
$$\gamma = 120^\circ$$



TRIGONAL

$$a = b = c$$

$$\alpha = \beta = \gamma \neq 90^\circ$$



MONOCLINIC

$$a \neq b \neq c$$

$$\alpha = \gamma = 90^\circ$$

$$\beta \neq 120^\circ$$



TRIGLONIC

$$a \neq b \neq c$$

$$\alpha \neq \beta \neq \gamma \neq 90^\circ$$



4 Types of Unit Cell

P = Primitive

I = Body-Centred

F = Face-Centred

C = Side-Centred

+

7 Crystal Classes

→ 14 Bravais Lattices

	<i>Mixed powders</i>	<i>Coprecipitation</i>	<i>Sol-gel</i>	<i>Hydrothermal</i>	<i>Spray and freeze drying</i>
State of development	Commercial	Commercial	Commercial; research and development	Demonstration	Demonstration
Size of particle (nm)	> 1000	> 10	> 10	> 100	> 10
Homogeneity	Poor	Good	Very good	Very good	Very good
Purity	Poor	Very good	Excellent	Very good	Excellent
Temperature of calcination (°C)	> 1000	500–1000	500–1000	80–374	> 150
Agglomeration	Moderate	High	Moderate	Low	Low
Costs	Low to moderate	Moderate	Moderate to high	Moderate	Moderate to high